

# **Carbon nanotubes as catalysts for catalytic wet peroxide oxidation of highly concentrated phenol solutions: towards process intensification**

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## Abstract

Commercial multi-wall carbon nanotubes with different properties (2 samples from Sigma-Aldrich, SA1 and SA2; 1 sample from Nanocyl, NC; and 2 samples from Shenzhen Nanotech, SZ and LSZ), and SA2 modified by hydrothermal treatment with concentrated sulfuric acid (SA2-H), were tested as catalysts in wet peroxide oxidation. Phenol was selected as model compound since represents a class of noxious compounds for human health and for the environment and, due to this, phenol is typically considered in wastewater treatment studies. The experiments were carried out under the following intensified conditions: phenol concentration =  $4.5 \text{ g L}^{-1}$ , hydrogen peroxide concentration =  $25 \text{ g L}^{-1}$ , catalyst load =  $2.5 \text{ g L}^{-1}$ , pH = 3.5, T = 353 K and 24 h.

The results demonstrated that phenol is poorly adsorbed in this type of carbon materials (11 % as maximum when using the NC sample). However, in the catalytic experiments, complete removal of phenol is achieved when using some of the carbon nanotubes (SA1, NC and SA2), together with a remarkable total organic carbon removal (77, 69 and 67 %, respectively). These materials have the less pronounced acidic character, which is often considered favorable for oxidation reactions in advanced oxidation processes and may explain the higher performance of SA1, NC and SA2 regarding the other materials. Leaching of Fe species into the solution was also observed in all cases (that can also have some influence on the degradation of phenol), SA1 leading to the highest concentration of Fe species leached ( $26 \text{ mg L}^{-1}$ ), followed by SA2 ( $2 \text{ mg L}^{-1}$ ) and NC ( $1 \text{ mg L}^{-1}$ ).

Considering the lower Fe leaching levels observed for SA2 and NC, these catalysts were then tested in consecutive reusability cycles. SA2 showed a superior performance than NC, however, temperature programmed desorption, as well as thermogravimetric analysis, suggested that the carbon material is oxidized by hydrogen peroxide at the employed conditions and/or that carboxylic acids are adsorbed on the catalyst surface after consecutive runs (mainly after the first use). However, only a slight decrease of the catalyst activity was observed.

*Keywords:* Catalytic wet peroxide oxidation; Carbon nanotubes; Phenol; Highly polluted effluents; Intensified process conditions.

## 1. Introduction

Organic pollutants like phenol and its derivatives appear in wastewaters from pharmaceutical, paper, petrochemical and from many other industries. These compounds are very toxic and difficult to eliminate from wastewaters by conventional biological processes, in particular when they are present in high concentrations (1-10 g L<sup>-1</sup>) [1]. In the quest to solve this problem, different treatments have been studied based on physical and chemical processes (e.g., flocculation, precipitation, adsorption on activated carbon, ozonation, chlorination and coagulation) [2]. Advanced oxidation processes (AOPs) have been particularly investigated among the chemical treatments [3-5].

AOPs are conceptually characterized by the production of hydroxyl radicals (HO<sup>•</sup>), which are very reactive species capable to oxidize a wide range of organic compounds and to reduce the toxicity of many effluents. Most of these processes can be operated at (or close to) ambient temperature and atmospheric pressure [6]. Different oxidizing agents (typically hydrogen peroxide, ozone or/and oxygen) can be considered depending on the process [7]. Particularly, hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) – a colorless and non-toxic compound – is a powerful oxidizing agent that easily decomposes into environmental friendly products (i.e. water and oxygen), following Eq. (1).



If a suitable catalyst is used, the decomposition of H<sub>2</sub>O<sub>2</sub> may proceed selectively through the formation of the highly reactive HO<sup>•</sup> radicals. This process is known as catalytic wet peroxide oxidation (CWPO). The classical Fenton process is one of the most known homogeneous AOPs, where a mixture of H<sub>2</sub>O<sub>2</sub> and Fe<sup>2+</sup> ions are employed at low pH (2.5 - 3.0) to promote the decomposition of H<sub>2</sub>O<sub>2</sub> into HO<sup>•</sup> radicals, this process being considered one particular case of CWPO (i.e. a specific catalyst at specific operating conditions). Still, heterogeneous catalysts can be easier separated from the treated solution when compared to homogeneous catalysts,

which is an important advantage relatively to the homogenous route [3]. Taking this into consideration, different supports, like activated carbons, pillared clays, zeolites, carbon xerogels and carbon nanotubes, have been employed in the last two decades to prepare transition-metal supported catalysts for CWPO [4, 8-14]. However, the loss of activity due to leaching of metal species when using heterogeneous catalysts, as well as further separation of these species from the treated water (when in quantities larger than those allowed by local Directives), are some of the arising difficulties in the use of transition-metal based catalysts. In order to overcome these drawbacks, metal-free carbon materials have been also tested as catalysts in CWPO, revealing promising activities [15-19].

Carbon nanotubes (CNT) have interesting properties when they are compared with other carbon materials, such as low mass transfer limitations, high level of ordering and mechanical resistance, superior electronic properties and relatively high thermal stability in oxidizing conditions. CNT are often produced by chemical vapour deposition (CVD) using metal nanoparticles as catalysts (such as Fe, Co, Ni, Cu, Au, Ag, Pt and Pd). In this catalytic method of synthesis, a hydrocarbon gas decomposes leading to the formation and growth of CNT on the top surface of the catalytic nanoparticles [20]. It is thus natural to find metal nanoparticles in the composition of commercial CNT. These metal species (especially Fe) are able to act as catalysts in the generation of HO<sup>•</sup> radicals from H<sub>2</sub>O<sub>2</sub> decomposition, as previously shown for commercial graphite [19]. Therefore, in addition to the recognized intrinsic catalytic activity of carbon materials, the effect of these metal nanoparticles on CWPO performance have to be considered when using CNT as catalysts on their own for CWPO processes.

In the present work, six different commercial CNT samples were compared as catalysts for the CWPO process. A highly concentrated phenol (4.5 g L<sup>-1</sup>) solution was considered as model system, in order to simulate highly polluted wastewaters and to maximize the efficiency of H<sub>2</sub>O<sub>2</sub> consumption, which is known to be favoured by high phenol/carbon mass ratios [21]. Under these conditions, the carbon surface is expected to stay largely covered by the organic

molecules, reducing the occurrence of parasitic scavenging reactions on the carbon surface and, consequently, increasing the degradation and mineralization of phenol. The stability of the catalysts that revealed better performances in screening experiments was further assessed in consecutive runs, an issue of relevance for actual applications of the CWPO process.

## 2. Experimental

### 2.1. Chemicals

Phenol was obtained from Sigma–Aldrich (99 wt. %). Hydrogen peroxide solution (30 %, w/w), *p*-benzoquinone (99.5 wt. %) and catechol (98 wt. %) were purchased from Fluka. Hydroquinone (99 wt. %), resorcinol (99 wt. %), titanium(IV) oxysulphate (~ 15 wt. % in dilute sulfuric acid, 99.99 % trace metals basis) and hydrochloric acid (37 wt. %) were purchased from Sigma-Aldrich. Sulphuric acid (95 wt. %) and methanol (99.9 wt. %) were obtained from VWR PROLABO Chemicals. All the solutions were prepared with distilled water.

### 2.2. Carbon nanotubes (CNT)

Six different samples of commercial multi-wall carbon nanotubes (MWCNT) were considered in this work, namely: **(i)** SA1 / Sigma-Aldrich, ref. 677248 (> 90 % carbon basis, O.D. x I.D. x L: 10-15 nm x 2-6 nm x 0.1-10 μm); **(ii)** SA2 / Sigma-Aldrich, ref. 724769 (> 95 % carbon basis, O.D. x L : 6-9 nm x 5 μm); **(iii)** NC / NANOCYL™, ref. NC3100 (> 95 % carbon basis, average diameter of 9.5 nm and length of 1.5 μm); **(iv)** SZ / Shenzhen Nanotech, ref. MWCNT-10 (> 97 % carbon basis, O.D. x L: < 10 nm x 5-15 μm); **(v)** LSZ / Shenzhen Nanotech, long CNTs with ref. L-MWCNT-60100 (> 97 % carbon basis, O.D. x L: 60-100 nm x 5-15 μm); **(vi)** SA2-H, resulting from the hydrothermal treatment of SA2 (10 g L<sup>-1</sup>) with concentrated sulfuric acid (18 mol L<sup>-1</sup>) during 3 h at 423 K. The recovered solids

were further thoroughly washed with distilled water until the neutrality of the rinsing waters was reached and dried in an oven for 18 h at 383 K.

### 2.3. Characterization techniques

The catalysts were characterized by different techniques. The textural properties were determined from the N<sub>2</sub> adsorption-desorption isotherms at 77 K, obtained in a Quantachrome NOVA 4200e adsorption analyzer. The specific surface area ( $S_{\text{BET}}$ ), pore volume ( $V_{\text{total}}$ ) and micropore volume ( $V_{\text{mic}}$ ) were determined using the t-method and the BJH pore distribution [22-23].

The pH of point of zero charge ( $\text{pH}_{\text{PZC}}$ ) was determined by pH drift tests, following the procedure described elsewhere [24]. Namely, five solutions with varying initial pH were prepared using HCl and NaOH solutions (0.02 mol L<sup>-1</sup> and 1.0 mol L<sup>-1</sup>) and NaCl (0.01 mol L<sup>-1</sup>) as electrolyte. 50 mL of each solution was contacted with 0.15 g of carbon sample and the suspension stirred for 24 h before the equilibrium pH was measured. The  $\text{pH}_{\text{PZC}}$  value of each carbon sample was determined by intercepting the obtained final pH vs. initial pH curve with the straight line final pH = initial pH [25-26].

Temperature programmed desorption (TPD) analysis was performed in a fully automated AMI-300 catalyst characterization instrument (Altamira Instruments), equipped with a quadrupole mass spectrometer (Dymaxion, Ametek). The carbon sample (0.10 g) was placed in a U-shaped quartz tube inside an electrical furnace and heated at 5 K min<sup>-1</sup> up to 1073 K using a constant flow rate of helium (25 cm<sup>3</sup> min<sup>-1</sup>). The mass signals  $m/z = 28$  and 44 were monitored during the thermal analysis, the corresponding TPD spectra being obtained. CO and CO<sub>2</sub> were calibrated at the end of each analysis with the respective gases [27].

Thermogravimetric analysis (TGA) was performed using a Netzsch STA 409 PC equipment. The sample powders were heated in air (flow = 50 cm<sup>3</sup> min<sup>-1</sup>) from 323 to 1273 K at 10 K min<sup>-1</sup>.

Scanning electron microscopy (SEM) images were obtained using a FEI Quanta 400FEG ESEM/EDAX Genesis X4M instrument equipped with an Energy Dispersive Spectrometer (EDS).

X-ray diffraction (XRD) analysis was performed in a PANalytical X'Pert MPD equipped with a X'Celerator detector and secondary monochromator (Cu K $\alpha$   $\lambda$  = 0.154 nm; data recorded at a 0.017° step size).

The amount of Fe species in the CNT was determined by atomic absorption analysis of the solution resulting from the acidic digestion of the samples. Namely, each sample was diluted in distilled water (5 mL) to which concentrated hydrochloric acid (12 mL) and concentrated nitric acid (4 mL) were added. The resulting solution was heated at 421 K during 2 h in order to promote the sample digestion, being afterwards cooled at room temperature and the remaining solids removed using a cellulose nitrate filter. The Fe content of the solution was analyzed by an atomic absorption spectrophotometer (EAA GBC 932 AB Plus), using an hollow cathode lamp (Photron P826).

#### *2.4. Adsorption and catalytic wet peroxide oxidation experiments*

The experiments were performed in a well-stirred batch glass reactor (250 mL) equipped with a condenser, and immersed in a water bath with temperature control. The reactor was loaded with 50 mL of a 4.5 g L<sup>-1</sup> phenol solution with the pH adjusted to 3.5 (with a 1.0 mol L<sup>-1</sup> HCl solution) and heated up to the desired temperature. All the experiments were conducted during 24 h at 353 K, considering an adsorbent/catalyst load of 2.5 g L<sup>-1</sup>. In the CWPO runs, a calculated volume of H<sub>2</sub>O<sub>2</sub> (30 wt. %) was injected into the system after catalyst addition, in order to reach the desired H<sub>2</sub>O<sub>2</sub> concentration of 25 g L<sup>-1</sup> (corresponding approximately to the stoichiometric amount needed to completely mineralize phenol), that moment being considered as  $t_0 = 0$  min. Blank experiments, without any catalyst, were also carried out to assess possible non-catalytic oxidation reactions promoted by H<sub>2</sub>O<sub>2</sub>. Adsorption runs (in the absence of H<sub>2</sub>O<sub>2</sub>)



were also performed with the CNT samples at the same temperature and pH. Selected experiments were performed in triplicate, in order to assess reproducibility and error of the experimental results. It was found that the confidence interval was never superior to 2%, considering 99% certainty.

### *2.5. Analytical methods*

The concentration of phenol and other aromatic compounds were analyzed by high performance liquid chromatography (HPLC) using a Hitachi Elite LaChrom apparatus equipped with a diode array detector (L-2450) and solvent delivery pump (L-2130). The stationary phase consisted in a Purospher Star RP-18 column (250 mm x 4.6 mm, 5  $\mu$ m particles) working at room temperature. The method starts with an isocratic method of water (C): methanol (B) (70:30) at a flow rate of 1 mL min<sup>-1</sup> followed by a linear gradient step to C:B (37:63) in 20 min. Finally, the initial conditions were re-established in a 1 min gradient step and the C:B (70:30) mixture was isocratically eluted for 7 min. The organic compounds were analyzed in a diode array detector at wavelengths from 210 to 290 nm.

The concentration of Fe species leached at the end of the CWPO experiments was determined by atomic absorption, using an atomic absorption spectrometer (Varian Spectra 220). The concentration of H<sub>2</sub>O<sub>2</sub> was evaluated by a colorimetric method using an UV/VIS spectrophotometer (UV Vis Jasco V-560), adapting the procedure described elsewhere [16]. The total organic carbon (TOC) of the samples was analyzed in a Shimadzu TOC-5000A apparatus.

## **3. Results and discussion**

### *3.1. Characterization of the CNT samples*

The textural characterization of the CNT samples was carried out by N<sub>2</sub> adsorption-desorption isotherms, the results being shown in Table 1. The sample SA2 has the highest specific surface area ( $S_{\text{BET}}$ ) and total pore volume ( $V_{\text{total}}$ ), the  $S_{\text{BET}}$  corresponding to the

non-microporous surface area ( $V_{\text{micro}} = 0 \text{ cm}^3 \text{ g}^{-1}$ ). Although lower  $S_{\text{BET}}$  and  $V_{\text{Total}}$  values were obtained, samples SA1, SA2-H and NC reveal quite similar textural properties relatively to SA2. Regarding the commercial MWCNT from Shenzhen Nanotech, SZ and LSZ, these were found to present low specific surface areas and total pore volumes when compared with all the other materials.

**TABLE 1**

The surface chemistry characterization was performed by TPD, a popular thermal analysis method for the characterization of oxygen groups on the surface of carbon materials. These oxygen groups decompose with temperature, being evolved as CO and/or CO<sub>2</sub>. The release of CO (between 673 to 1273 K) corresponds to the decomposition of carboxylic anhydrides, phenols and quinones, while the release of CO<sub>2</sub> (between 473 to 1073 K) is attributed to the decomposition of carboxylic acids, lactones and carboxylic anhydrides [28]. The results obtained by TPD analysis of the CNT samples are also shown in Table 1, namely in terms of CO and CO<sub>2</sub> amounts, as well as CO/CO<sub>2</sub> ratio and molecular oxygen percentage. These results show that NC has the highest amount of oxygen groups released as CO, while the lowest amount was found for SZ. Regarding CO<sub>2</sub>, LSZ shows the highest value for the release of CO<sub>2</sub>, while SA1 presents the lowest. The CO/CO<sub>2</sub> ratio is highest for SA1 (5.6), followed by NC (5.4) and SA2 (4.5), suggesting that these samples present the less pronounced acidic character, i.e. CO/CO<sub>2</sub> ratios well above the other samples ( $\leq 2.2$ ).

Considering the catalytic experiments performed with the commercial CNT samples (as shown later in Section 3.3), the two materials showing the best performance in the removal of phenol by CWPO (i.e., SA2 and NC) were further characterized. In this context, in order to better understand the surface chemistry of the materials, the pH at the point of zero charge ( $\text{pH}_{\text{PZC}}$ ) was determined. SA2 reveals a slight acidic nature, with a  $\text{pH}_{\text{PZC}}$  of 5.1, and NC reveals a slight basic nature, with a  $\text{pH}_{\text{PZC}}$  of 8.9. The morphology of selected CNT samples (SA2 and NC) was investigated by SEM (Figures 1a and 1b, respectively). The SEM micrographs and the

corresponding EDS spectra show large agglomerates of CNT in both samples and that only carbon and oxygen are detected by EDS analysis.

### FIGURE 1

#### 3.2. Adsorption experiments

Adsorption experiments were carried out to assess the capacity of the different CNT samples to adsorb phenol, and thus understand the influence of adsorption in the global performance obtained by CWPO (i.e., in experiments in the presence of H<sub>2</sub>O<sub>2</sub>). The corresponding time-evolution of phenol concentration obtained in adsorption experiments, performed under the conditions referred in Section 2.4, is shown in Figure 2.

### FIGURE 2

According to Figure 2, a higher adsorption of phenol was observed in 24 h when the NC sample was employed, followed by  $SZ > SA1 > SA2-H \approx SA2 > LSZ$ . For better comparison between the different materials, Table 2 shows detailed data of phenol adsorption removal after 24 h. It is observed that NC presents the highest phenol adsorption removal (198 mg g<sup>-1</sup>) while LSZ presents the lowest (68 mg g<sup>-1</sup>), which seems to be related with their respective surface areas (256 and 51 m<sup>2</sup> g<sup>-1</sup>, respectively, as observed in Table 1). Even so, the adsorption of phenol is not always proportional to S<sub>BET</sub>. For example, the specific surface area of SA2-H is higher comparatively to SZ (242 and 41 m<sup>2</sup> g<sup>-1</sup>, respectively), but SA2-H shows less adsorption than SZ in 24 h. The four possible locations of sites for the adsorption of pollutants on CNT can be classified as: (i) inside channels (inner diameter of the tubes), (ii) interstitial channels (space between different CNT in a bundle), (iii) external groove and (iv) external surface (both related with the outer CNT in a bundle). In addition, different mechanisms may act simultaneously (e.g., electrostatic interactions, hydrophobic interactions,  $\pi$ - $\pi$  bonds and hydrogen bonds) and the accessibility of the pollutant to these sites can be affected by functional groups. In this

context, the prediction of organic chemical adsorption on CNTs is still a challenging task [29], in particular when the differences in adsorption results are not significant (Figure 2).

## TABLE 2

### 3.3. CWPO experiments

The different CNT samples were tested in CWPO experiments, carried out under the conditions referred in Section 2.4. The results obtained are given in Figure 3. The non-catalytic results (i.e. reaction experiments performed only with H<sub>2</sub>O<sub>2</sub>) are also included for comparison.

## FIGURE 3

From the analysis of Figure 3, it is possible to conclude that all catalysts are able to remove more than 80 % of the initial phenol content after 24 h of reaction (as also shown in Table 2). The best performance was obtained with the catalyst SA1, followed by NC and SA2. These three CNTs show the highest activity, with 100 % phenol removal being obtained. On the other hand, SZ, LSZ and SA2-H show the lowest catalytic activity among all the tested materials. The phenol removals after 24 h by adsorption and CWPO can be all compared in Table 2.

The highest phenol removal rates (SA1 > NC > SA2, in Figure 3) seems to be well related with the CO/CO<sub>2</sub> ratios of the materials (5.6 > 5.4 > 4.5, respectively, as observed in Table 1). All these materials also presents quite high BET surface areas ( $\geq 200 \text{ m}^2 \text{ g}^{-1}$ ). However, it is also important to consider that in some cases the results can be explained by the presence of metal particles in the composition of the commercial CNT tested in this work. For instance, according to the manufacturers, SA1 was produced by chemical vapour deposition using iron particles as catalyst (also known as active catalysts in CWPO), whereas SZ and LSZ were synthesized using Co and Mo catalysts (much less active in CWPO). In the particular case of NC, the main metal impurities are Fe and Co, as referred elsewhere [30]. In order to assess their possible influence, the Fe species leached into the solution were determined at the end of the CWPO runs. The corresponding results are shown in Figure 4. As observed, the concentration of Fe species in the

solution is significantly higher for SA1, namely in the following order: SA1 (26.3 mg L<sup>-1</sup>) >> SA2 (2.1 mg L<sup>-1</sup>) > NC (1.0 mg L<sup>-1</sup>) > SA2-H ≈ SZ (0.6 mg L<sup>-1</sup>) > LSZ (0.1 mg L<sup>-1</sup>).

Fe species are known to catalyze H<sub>2</sub>O<sub>2</sub> decomposition into reactive HO• radicals in acid solutions [31-34]. In this mechanism, regarding the radicals generated, Fe<sup>2+</sup> and H<sub>2</sub>O<sub>2</sub> lead to the formation of HO• and Fe<sup>3+</sup>, and then Fe<sup>3+</sup> is converted into Fe<sup>2+</sup> through the formation of hydroperoxyl radicals (HO<sub>2</sub>•). For the CNT tested in this work, these reactions can occur both at the catalyst surface and in solution, since the concentration of Fe species leached into the solution (SA1 > SA2 > NC) does not correlate with the extents observed in Figure 3 for the degradation of phenol (SA1 > NC > SA2).

#### FIGURE 4

Figure 4 also shows the total organic carbon (TOC) conversions obtained at the end of the CWPO runs. As observed, the level of mineralization increases with the phenol removal. SA1 presents the highest TOC conversion (77 %), followed by NC (69 %) > SA2 (67 %) > SA2-H (58 %) > LSZ (46 %) > SZ (45 %). As in the case of phenol conversions, TOC removals does not correlate directly to Fe species leached into the solution.

Although phenol is completely removed with SA1, NC and SA2, a fraction of the initial TOC remains in the final aqueous solution. This suggests the formation of reaction intermediates, such as aromatic compounds (like hydroquinone, resorcinol, *p*-benzoquinone and catechol) and their oxidation by-products. Possible explanations for the incomplete TOC abatement may be (i) inhibition of effective H<sub>2</sub>O<sub>2</sub> decomposition to HO• radicals due to the presence of organic compounds on the catalyst surface (i.e. a competitive process between H<sub>2</sub>O<sub>2</sub> and the organic molecules for the active sites at the catalyst surface) [21]; (ii) thermal decomposition of H<sub>2</sub>O<sub>2</sub> during reaction, as described by Eq. (1) (although limited in the presence of a catalyst, it depends on the carbon texture and surface chemistry); and (iii) several other pathways avoiding effective usage of HO• radicals for degradation of phenol oxidation intermediates [16], such as those given in Eqs. (2) to (5). As described in these equations, the free radicals may react with

each other or may also react with H<sub>2</sub>O<sub>2</sub>. Generally speaking, a high concentration of H<sub>2</sub>O<sub>2</sub> does not necessarily leads to higher TOC removal in CWPO, and the use of an excess of oxidant is often useless in that regard [35-39]. In fact, as observed in Figure 4, the H<sub>2</sub>O<sub>2</sub> conversions are quite high regardless the catalyst tested and the respective TOC abatement, suggesting the occurrence of the parasitic reactions described in Eq. (2) to (5).

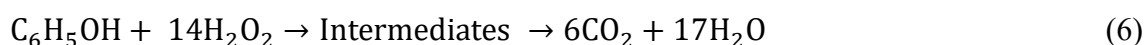


Phenol can be degraded by HO<sup>•</sup> radicals, typically through an electrophilic addition to the aromatic ring [40]. Due to the influence of the phenolic – OH group, this addition will occur mainly in selective *ortho* and/or *para* positions, leading to the formation of catechol and hydroquinone, respectively [40]. Nevertheless, the formation of resorcinol is also expected due to residual electrophilic addition in selective *meta* position [21, 41]. Furthermore, hydroquinone is known to be very easily oxidized into *p*-benzoquinone [42]. In order to further explore the reaction mechanism, the occurrence of some possible aromatic intermediates resulting from phenol CWPO was investigated as described in Section 2.5. SA2 and NC were selected for this study, since higher TOC removals are obtained when they are employed in the CWPO process (SA1 was discarded for further studies due to the high leaching observed). As expected, hydroquinone, resorcinol, *p*-benzoquinone and catechol were detected when using both catalysts, the corresponding evolution being shown in Figures 5a and 5b, for SA2 and NC catalysts, respectively. As it can be seen, the maximum concentrations of the intermediates are generally obtained after ca. 1.5 h of reaction, then decreasing significantly until residual concentrations being reached at the end of the CWPO experiments performed with the highly polluted phenol solution (4.5 g L<sup>-1</sup>) during 24 h. This suggests that other by-products (such as

low weight carboxylic acids) should also be present in solution at the end of the CWPO runs, resulting from the aromatic ring cleavage [21]. Furthermore, pH measurements performed at the end of the CWPO runs revealed that the solution pH decreases from 3.5 to ca. 2.5 during the CWPO process (24 h), also suggesting the formation of carboxylic acids.

### FIGURE 5

The concentration of the aromatic intermediate compounds (Figure 5) increases/decreases according to the reaction described by Eq. (6), and among them the highest concentration was observed for catechol (followed by *p*-benzoquinone > hydroquinone > resorcinol). The concentrations of *p*-benzoquinone and hydroquinone (formed by *para*-hydroxylation) were ca. 20-40 % to that of catechol. Resorcinol (formed by *meta*-hydroxylation) was present only in trace amounts in the catalytic run carried out with SA2, while a concentration of approximately 20 % to that of catechol was detected in the run with NC.



Summarizing, a graphical representation of the mechanism for phenol CWPO is given in Figure 6, which has been widely described in literature for phenol oxidation by AOPs [43].

### FIGURE 6

#### 3.4. Catalyst stability and reusability studies

Catalysts SA2 and NC were recovered by filtration after the CWPO experiments in order to assess their stability and reusability characteristics. The materials were washed, dried at room temperature for 12 h and then at 393 K for 3 h. Afterwards, the catalysts were reused with fresh phenol solutions. Figures 7a and 7b show the results obtained with SA2 and NC, respectively, including phenol and TOC conversions, leaching of Fe species and the  $X_{\text{TOC}}/X_{\text{H}_2\text{O}_2}$  ratio after 24 h, a parameter that defines the efficiency of  $\text{H}_2\text{O}_2$  consumption in the CWPO process. It is observed, for both catalysts, that the degradation of phenol and TOC decreases slightly with the reusing cycles. Notwithstanding, the conversions still remain high. Regarding the concentration

of Fe species leached into solution, a significant decrease is observed from the first to the second run in the case of SA2. However, this decrease is not followed by a loss of efficiency of the catalyst. This evidence may indicate that although Fe species are being transferred to the solution with a corresponding possible contribution of homogeneous catalysis in the generation of HO<sup>•</sup> radicals, and subsequent phenol degradation, the catalyst unequivocally possesses intrinsic heterogeneous activity for the CWPO process. Relatively to NC, the decrease of phenol conversion from the first to the second run is slightly higher when compared to that of SA2. Nevertheless, despite the negligible Fe leached to the solution in the third run ( $< 0.1 \text{ mg L}^{-1}$ ), TOC removal is barely affected during its successive reuse.

### FIGURE 7

Therefore, the apparent slight loss of activity observed with the SA2 and NC catalysts may be partially explained by adsorption of the pollutant at the catalyst surface in the first run, by deposition of some other species (such as reaction by-products) on the catalyst surface [21], or even by the decrease of the iron content of the samples during the first CWPO run (namely from 0.053 wt.% to 0.041 wt.% in the case of SA2, and from 0.049 wt.% to 0.047 wt.% for the run performed with NC; these low values presenting however a high experimental uncertainty). In order to explore the possible deposition of organic compounds on the catalyst surface, TPD analysis was performed for the original SA2 (Figures 8a and 8b) and NC (Figures 8c and 8d) materials as well as for the respective samples recovered after the first and the third reaction runs, in terms of CO (Figures 8a and 8c) and CO<sub>2</sub> (Figures 8b and 8d) evolution. The most important finding is that the amount of carboxylic acids (decomposing at the lower temperatures as CO<sub>2</sub> [28]) increases after the CWPO runs, while the other groups evolved as CO<sub>2</sub> or even CO are not so significantly affected. Thus the CO/CO<sub>2</sub> ratio decreases upon catalyst reuse (namely from 4.5 to 0.5 in the case of SA2 and from 5.4 to 0.9 in NC), indicating that carboxylic acids are adsorbed on the catalyst surface or/and that the catalyst is oxidized by H<sub>2</sub>O<sub>2</sub> during the CWPO reactions generating mainly carboxylic acid groups. This effect is particularly



remarkable during the first reaction run. As a consequence, the adsorbed organic compounds can lead to the blockage of the active sites available for H<sub>2</sub>O<sub>2</sub> decomposition, while at the same time the introduction of oxygen electron-withdrawing groups can diminish the electron density at the carbon surface, also reducing the catalyst activity. Therefore, these changes can be responsible by the slight decrease in the catalysts activity in the successive reutilization experiments (Figure 7).

### FIGURE 8

In order to get more insights, TGA under air atmosphere was performed for the original SA2 catalyst and for the samples recovered after the first and the third reaction runs (Figure 9). The original catalyst shows quite high stability since its gasification starts at high temperatures (773 K). However, the samples after the first and the third runs started to lose weight around 473 K, in agreement with TPD analysis (Figure 8b). Therefore, this can be attributed to oxidation of the adsorbed by-products or to the decomposition of surface oxygen groups generated during reaction, thus suggesting that these phenomena are the possible cause for the slight loss of activity observed with the catalysts upon reuse. Furthermore, the influence of CWPO on the CNT structure was also assessed. For that purpose, XRD analysis of SA2 and NC (before and after CWPO) was performed, the resulting diffractograms being shown in Figures 10a and b, respectively. The XRD profiles are analogous to that found for other commercial CNT samples [15]. In addition, for both SA2 and NC, similar XRD profiles are obtained before and after CWPO, suggesting no significant distortion of the CNT structure upon their use in the CWPO process.

Regarding the  $X_{\text{TOC}}/X_{\text{H}_2\text{O}_2}$  ratios reported in Figure 7, it is observed that this parameter presents similar values for the two catalysts in the successive reuses (ranging between 0.72 and 0.64), suggesting that a large percentage of the oxidizing agent is effectively used in the mineralization of phenol. Thus, with the results obtained in this work, it is concluded that SA2 and NC are catalysts with moderate stability for long-term reaction runs, able to promote the

CWPO of highly concentrated phenol solutions with a good efficiency of H<sub>2</sub>O<sub>2</sub> consumption, making these commercial materials suitable for industrial applications on wastewater treatment.

**FIGURE 9**

**FIGURE 10**

#### **4. Conclusions**

Commercial multi-wall carbon nanotubes with different properties were tested for the treatment of highly concentrated phenol solutions by catalytic wet peroxide oxidation. Considering phenol and total organic carbon removals, as well as the extent of Fe species leached into solution, the catalysts with best performance were SA2 (obtained from Sigma-Aldrich, ref.72476) and NC (obtained from NANOCYL, ref. NANOCYL™ NC3100). Aromatic reaction by-products like catechol, *p*-benzoquinone, hydroquinone and resorcinol were the compounds identified in higher concentrations. Based on reutilization experiments performed with SA2 and NC, it can be concluded that these materials are fairly stable, with a slight loss of activity being observed in three consecutive runs. The activity decrease of the catalysts was more likely ascribed to adsorbed organic compounds, such as low molecular weight carboxylic acids, which can block the sites for H<sub>2</sub>O<sub>2</sub> decomposition, but other possible explanations are the generation of carboxylic acid groups, which can reduce the electron density on the carbon surface of the carbon nanotubes, and the presence of metals in the catalysts.

#### **Acknowledgments**

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## TABLES

**Table1.** Textural properties and surface chemistry of the different carbon nanotubes: specific surface area ( $S_{\text{BET}}$ ,  $\pm 10 \text{ m}^2 \text{ g}^{-1}$ ), total pore volume ( $V_{\text{Total}}$ ,  $\pm 0.01 \text{ cm}^3 \text{ g}^{-1}$ ) and concentration of oxygen containing functionalities ( $\pm 20 \mu\text{mol g}^{-1}$ ) released as CO and CO<sub>2</sub> during TPD analysis.

Sample	$S_{\text{BET}}$ ( $\text{m}^2 \text{ g}^{-1}$ )	$V_{\text{total}}$ ( $\text{cm}^3 \text{ g}^{-1}$ )	CO ( $\mu\text{mol g}^{-1}$ )	CO <sub>2</sub> ( $\mu\text{mol g}^{-1}$ )	CO/CO <sub>2</sub>	O <sub>2</sub> (%)
SA1	200	1.5	594	107	5.6	1.3
SA2	291	3.2	785	174	4.5	1.8
SA2-H	242	2.9	750	344	2.2	2.3
NC	256	2.8	1003	186	5.4	2.2
SZ	41	0.17	390	238	1.6	1.4
LSZ	51	0.17	569	481	1.2	2.4

**Table 2.** Phenol removal after 24 h ( $\pm 1$  %) obtained by pure adsorption (Ads.) and CWPO under intensified conditions ( $[\text{phenol}] = 4.5 \text{ g L}^{-1}$ , catalyst load =  $2.5 \text{ g L}^{-1}$ ,  $T = 353 \text{ K}$  and  $\text{pH} = 3.5$ ) when using different carbon nanotubes.

Material	Phenol removal			
	Ads.	CWPO	Ads.	CWPO
	(%)	(%)	( $\text{mg g}^{-1}$ )	( $\text{mg g}^{-1}$ )
SA1	7.9	100	142	1800
SA2	4.7	100	85	1800
SA2-H	5.0	89	90	1602
NC	11	100	198	1800
SZ	9.0	83	162	1494
LSZ	3.8	84	68	1512



## FIGURE CAPTIONS

**Figure 1.** SEM micrographs and corresponding EDS spectra of (a) SA2 and (b) NC.

**Figure 2.** Normalized phenol concentration decay curves obtained in phenol adsorption runs performed with the different carbon nanotubes during 24 h. Adsorption conditions: [phenol] = 4.5 g L<sup>-1</sup>, adsorbent load = 2.5 g L<sup>-1</sup>, T = 353 K and pH = 3.5.

**Figure 3.** Normalized phenol concentration decay curves obtained in phenol CWPO runs performed with the different carbon nanotubes during 24 h. Reaction conditions: [phenol] = 4.5 g L<sup>-1</sup>, catalyst load = 2.5 g L<sup>-1</sup>, T = 353 K, pH = 3.5 and [H<sub>2</sub>O<sub>2</sub>] = 25 g L<sup>-1</sup>. The results obtained in the non-catalytic experiments are also shown for comparison.

**Figure 4.** Phenol, TOC and H<sub>2</sub>O<sub>2</sub> conversion (bars and squares/left axis) and concentration of Fe species leached (circles/right axis), after 24 h, in CWPO runs performed with the different carbon nanotubes.

**Figure 5.** Concentration of aromatic intermediates detected in the CWPO of phenol as a function of time when using the SA2 (a) and NC (b) catalysts.

**Figure 6.** Schematic representation for phenol conversion pathway in CWPO.

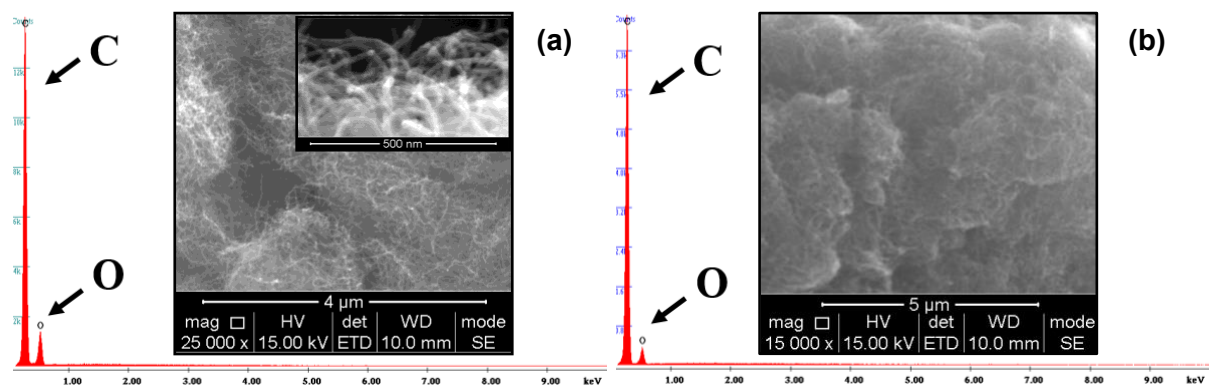
**Figure 7.** Phenol and TOC removal (bars/left axis), concentration of iron leached and  $X_{\text{TOC}}/X_{\text{H}_2\text{O}_2}$  (squares/right axis), after 24 h, in the series of three consecutive CWPO runs performed with the SA2 (a) and NC (b) catalysts.

**Figure 8.** TPD spectra before CWPO and after the 1<sup>st</sup> and the 3<sup>rd</sup> uses of the catalyst SA2 (a,b) and of the catalyst NC (c,d) in terms of CO (a,c) and CO<sub>2</sub> (b,d) evolution.

**Figure 9.** TGA of the catalyst SA2 before CWPO and after the 1<sup>st</sup> and the 3<sup>rd</sup> uses, obtained under air atmosphere with a 10 K min<sup>-1</sup> heating rate.

**Figure 10.** XRD spectra of (a) SA2 and (b) NC (before and after the CWPO process).

**FIGURE 1**



**FIGURE 2**

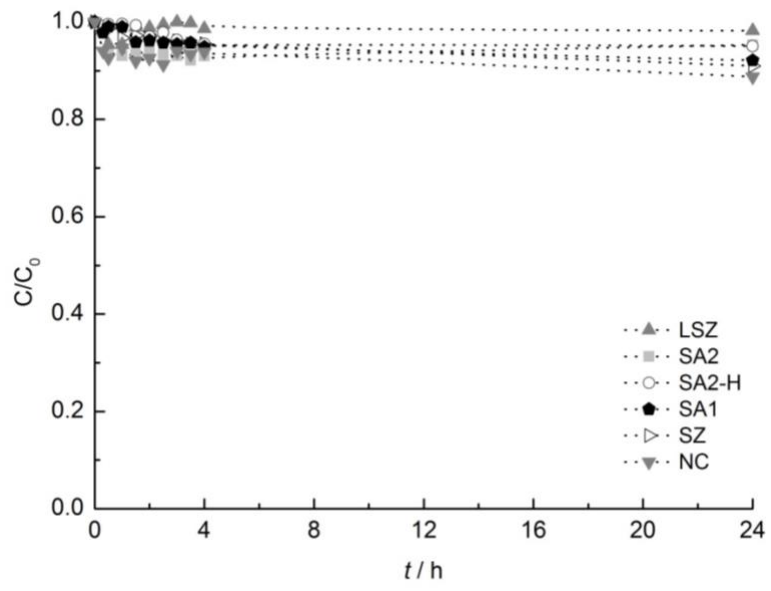
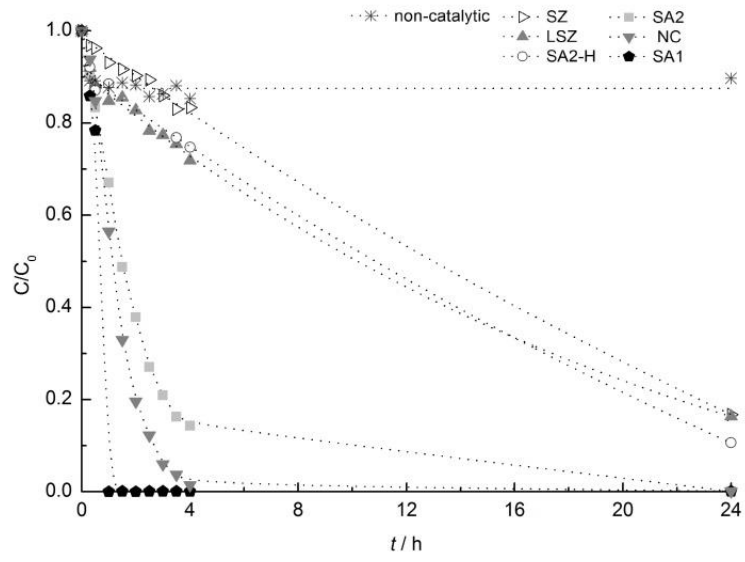
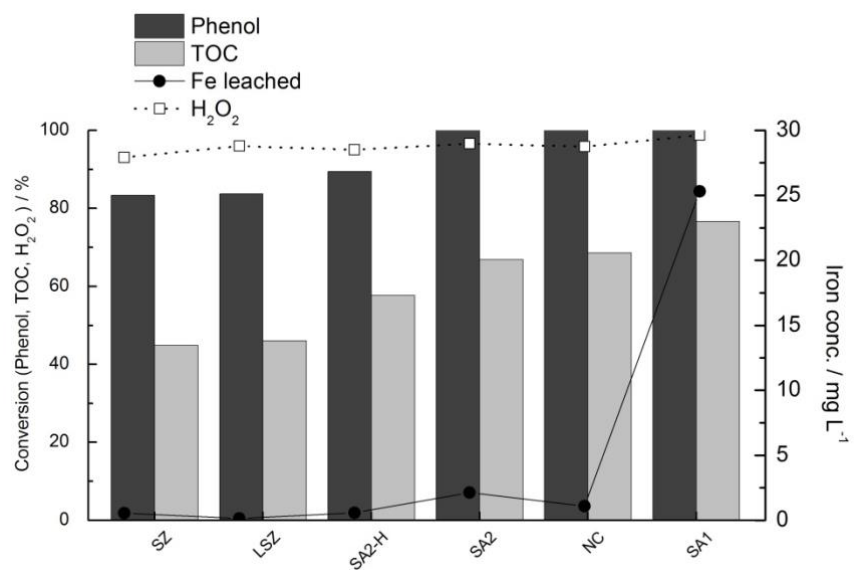


FIGURE 3



**FIGURE 4**



**FIGURE 5**

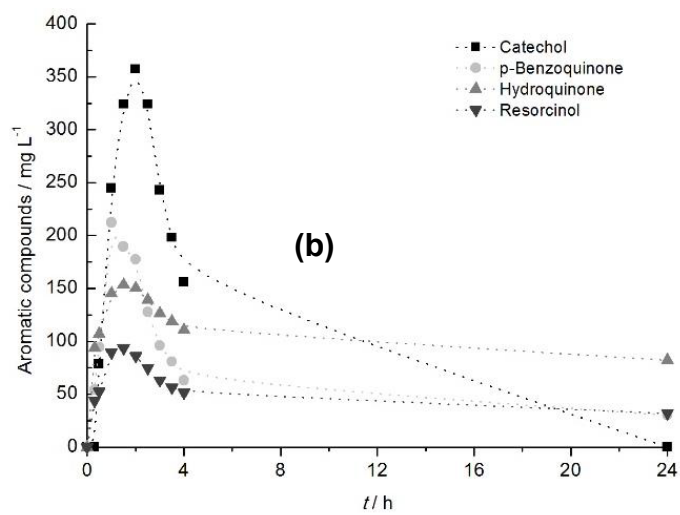
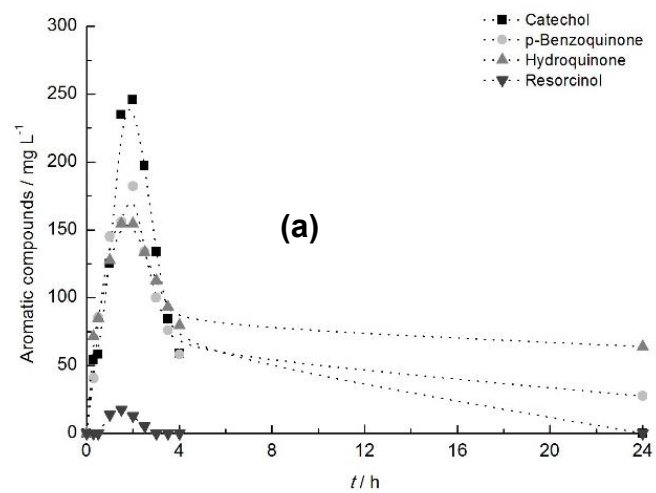
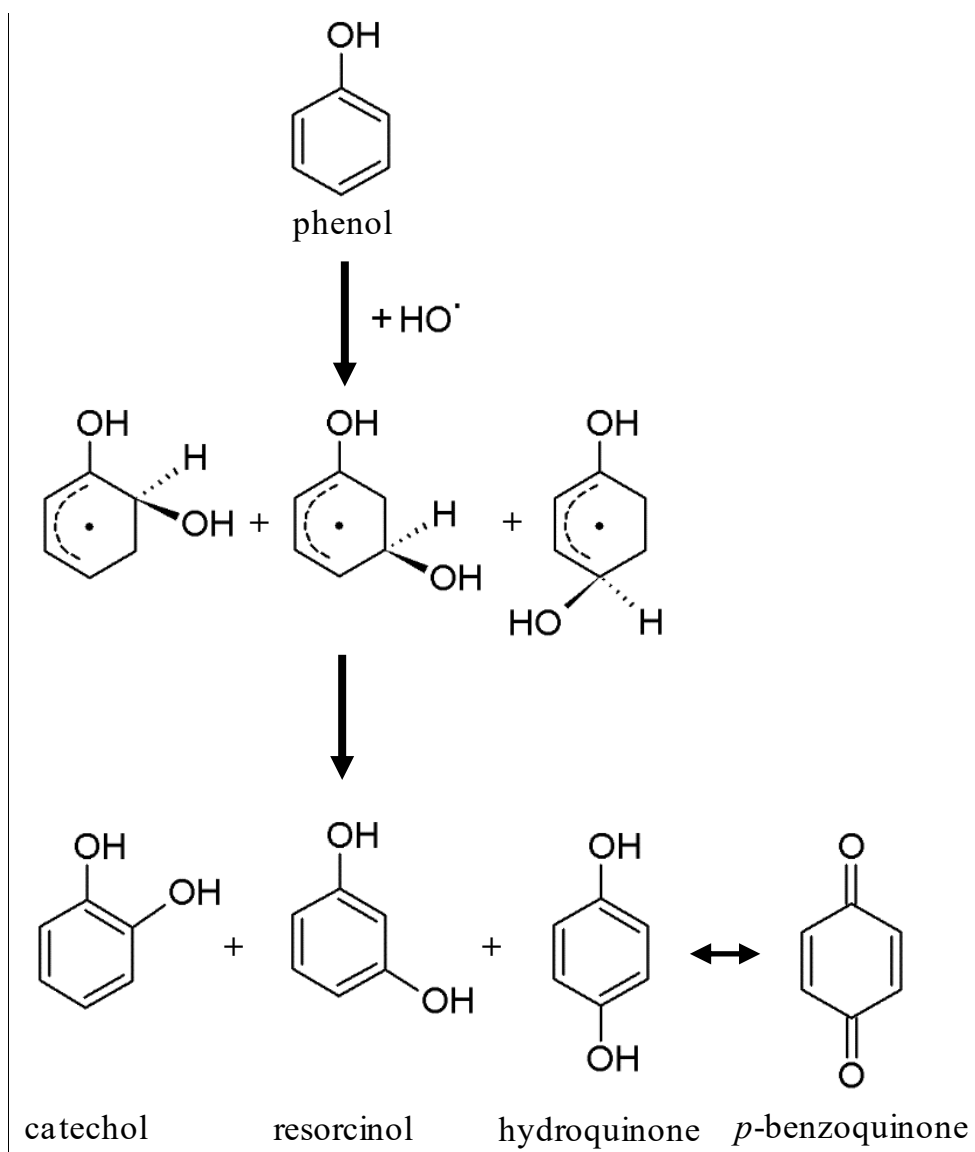
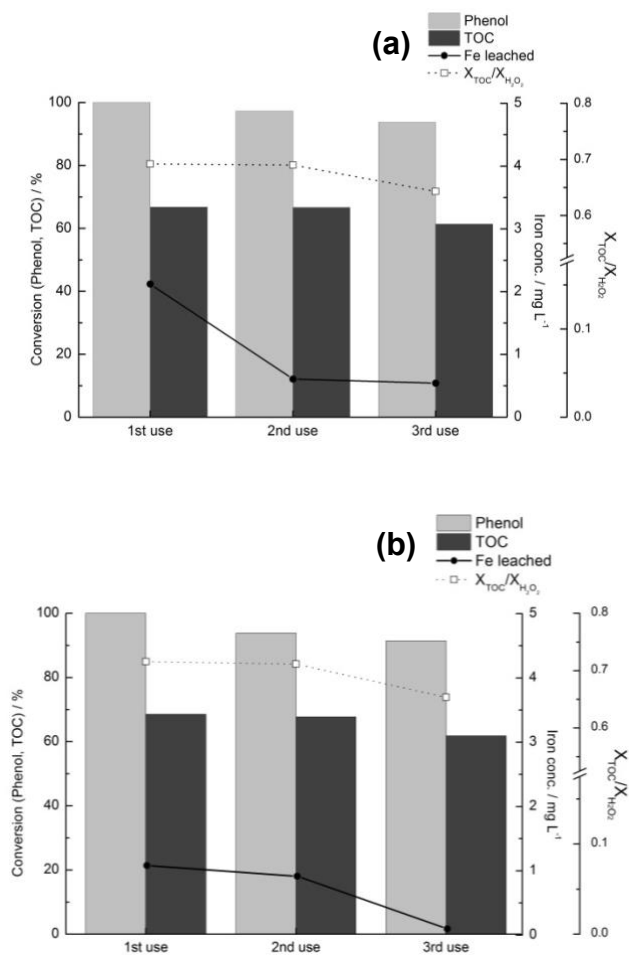


FIGURE 6

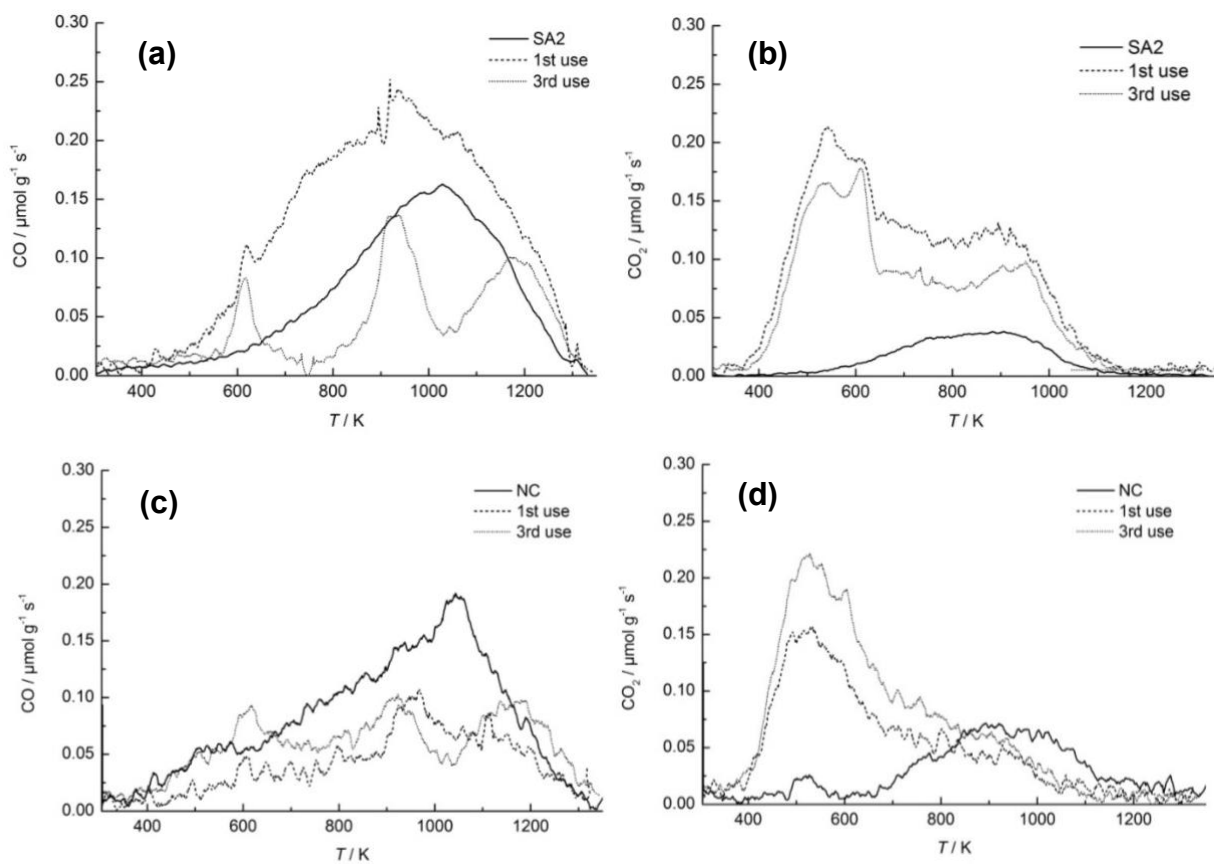




**FIGURE 7**



**FIGURE 8**



**FIGURE 9**

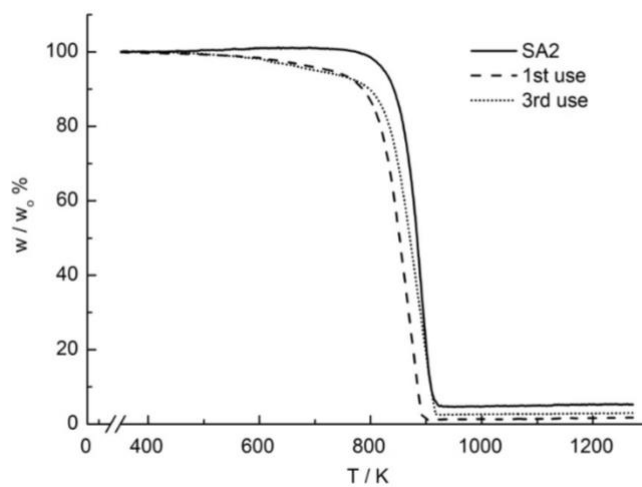


FIGURE 10

